

# AN ANALYSIS ON MICROWAVE PLASMA FLAME POWER SUSTAINABILITY: TEMPERATURE GRADIENT – THERMAL SPEED – FLAME GROWTH SPEED

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**Abstract.** *The generation and behavior of microwave plasma flame in a gasification reactor (MCw GASIFIER) is analyzed. Microwave plasma generation is at a frequency of 2450 MHz at atmospheric pressure. Air at the rates of 50 L/min and 100 L/min are used in the power (P) range of  $3000\text{ W} \leq P \leq 6000\text{ W}$ . Local instantaneous temperature  $T=T(y,t)$  measurements along the flame (y) are referred. The time-averaged temperature ( $T_y$ ) is calculated from the instantaneous data  $T(t)$ . The power sustainability of flame is estimated through defined parameters of temperature gradient (TG), thermal speed (VT) and flame growth speed (Vy).  $TG = dT_y / dy$  is a measure of flame thermal growth.  $VT = \Delta T_y / \Delta t$  indicates the local time averaged temperature gradient ( $\Delta T_y$  during the time ( $\Delta t$ ) for the increase of power ( $\Delta P$ ).  $Vy = VT/TG$  is the derived parameter. The existence of a linear relationship between Vy and VT for 50 L/min air flow is the confirmation of the modeling, sensitivity of flame generation and accuracy of the temperature measurements.*

**Keywords:** *Microwave Plasma Flame, Plasma Power, Flame Temperature Gradient, Flame Thermal Speed, Flame Growth Speed*

## 1. Introduction

It is known that ignition chemistry and its influence on combustion has a coupling with a dramatic problem of misfiring and failed ignition [1]. In order to solve this problem; microwave enhancement is used as an advanced ignition technology. The ignition delay associated with reaction kinetics can be reduced by means of high concentrations of radicals in plasma [2, 3]. Padala et al. 2017 [4] have conducted a study upon flame size measurements in a premixed propane-air mixture at varying amounts of air by a microwave-enhanced plasma. They paid attention to the minimum size of flame, flame speed and sustainability of flame from an initial spark kernel to a propagating form.

Somehow a similar study with a different methodology under the influence of a wide range of parameters for the determination of microwave plasma flame power sustainability is the topic of the paper.

The generation and control of microwave plasma flame the estimated dimensional characteristics and flame temperature measurements are given briefly in a previous paper of the authors [5, 6]. The generated microwave plasma flame is in use for the decomposition of solid wastes in the gasification reactor of MCw GASIFIER [7]. However the focus herein is on the analysis of microwave plasma flame growth as a counterpart of study [4]. The

analysis is founded on flame local instantaneous temperature measurements,  $T(y,t)$  along the plasma flame (y) under the influence of plasma environment gas rate and applied power (P). The generated flame is directed as a downflow jet leaving the complete assembly of plasma applicator with reactor head. Pure air in the closed gasification reactor at atmospheric conditions in the range of power (P);  $3000\text{ W} \leq P \leq 6000\text{ W}$  is considered since air-steam mixtures cause reduction in the size of flame. The analysis is through the introduction of parameters for flame power sustainability. The defined parameters of TG, VT, Vy are given in comparison with Padala et al's approach [4].

## 2. Material and Methods

MCw GASIFIER [5, 6] is an open cycle blower type set-up using microwave plasma generation and control system of MUEGGE (Table 1). The system is able to generate microwave plasma at a varying input power up to a maximum power of 6000 W at a frequency of 2450 MHz with the air as the plasma environment gas. The increment of power is having a sensitivity of 1%.

The generation and control of power (P) is by means of the software program of MUEGGE MX model. The utilized power supplier is MUEGGE MX6000D-110 K.

75

1 Table 1. MCw GASIFIER System Description 2

| SYSTEMS OF MCw GASIFIER                        | TYPE                                                                             | SUB-SYSTEMS(COMPO NENTS)                                                                                                                                 | CHARACTERISTIC S- FUNCTION                                                                                              | UTILIZED RANGE                                                                                         |
|------------------------------------------------|----------------------------------------------------------------------------------|----------------------------------------------------------------------------------------------------------------------------------------------------------|-------------------------------------------------------------------------------------------------------------------------|--------------------------------------------------------------------------------------------------------|
| MICROWAVE PLASMA GENERATION AND CONTROL SYSTEM | MUEGGE<br><br>(SOFTWARE PROGRAM: Muegge MX model control software)               | MX6000D-110K model power supplier<br><br>MH6000S-213BF model magnetron head (In combination with Isolator, 3-D Stub-Tuner, Wave Guide Plasma Applicator) | Generation of Power up to P= 6000 W<br><br>Generation, control and transmission of microwave signal to introduce plasma | 3000 W $\leq P \leq$ 6000 W<br><br>Sensitivity: 1% variation in power (P)<br><br>Frequency of 2450 MHz |
|                                                | Elimko E-PR-110 model data acquisition card                                      |                                                                                                                                                          |                                                                                                                         |                                                                                                        |
| GASIFICATION REACTOR                           | Custom-made fixed bed, cylindrical, swirling inlet of plasma gas at reactor head | Reactor head (In combination with plasma applicator)                                                                                                     | Height: 125 mm                                                                                                          |                                                                                                        |
|                                                |                                                                                  | Main body                                                                                                                                                | Height: 500 mm<br>Diameter: 81 mm                                                                                       | Local temperature measurements                                                                         |
| PLASMA ENVIRONMENT FEEDING SYSTEM              | Air Supplier:<br><br>Lupamat LKV 30/8 model screw compressor.                    | Flow rate measurement:<br><br>ALICAT MCR-250SLPM-D model mass flow controller is used                                                                    | Compressed air which has maximum 8 bar pressure and 4850 L/min flow<br>Uncertainty: 0.7 L/min                           | 50 L/min Air pure<br><br>100 L/min Air pure                                                            |

3

4 Air supplier is LUPAMAT LKV 30/8 model screw 25  
5 compressor in connection with ALICAT MCR- 26  
6 250SLPM-D model mass flow controller. Gasification 27  
7 reactor is a custom-made stainless steel cylindrical main 28  
8 body in combination with a reactor head and plasma 29  
9 applicator assembly having a length of 125 mm. 30  
10 Diameter of the reactor is 81 mm and a length of 500 mm. 31  
11 The reference line is the edge of plasma applicator 32  
12 resulting in a total length of 625 mm of the reactor 33  
13 assembly. Plasma environment gas – air inlet is directed 34  
14 from the reactor head as a swirling jet. Plasma applicator 35  
15 is in combination with the reactor head. Quartz glass tube 36  
16 located at the center of plasma applicator-reactor head 37  
17 assembly has a diameter of 3 cm and length of 5 cm. 38  
18 It is observed with the pictures of free- jet downflow 39  
19 plasma flame taken by a digital camera of SONY 40  
20 CYBERSHOT DSC-W220 12.1 that flame center is 41  
21 coincident with the axis of the quartz tube [5]. The 42  
22 recorded pictures were analyzed by using the digitizer 43  
23 tool of commercial ORIGIN PRO 8.5.1 software 44  
24 program. Although pointed end- conical and spreading

shapes are observed; the shape of flame can be approximated as a cylinder. In the covered  $P \geq 3000$  W, flame has a length (L) which is parallel to y;  $L \geq 25$  cm and a diameter (D) perpendicular to y;  $D \geq 3.5$  cm. A sample flame photograph is given in Fig. 1.

The generated microwave plasma flame was directed in the closed reactor at varying operational conditions and temperature measurements along the flame were conducted. B type (Pt18Rh-Pt) thermocouples having the measurement range of temperature up to 1820°C with a sensitivity of  $\pm 4$  °C were used. Thermocouples were located at 5 different locations of  $y = 175$  mm,  $y = 275$  mm,  $y = 375$  mm,  $y = 475$  mm and  $y = 575$  mm along the reactor wall. Thermocouple probes were immersed at 4 cm from the reactor wall such that probe tips were 0.5 cm apart from the reactor centerline. Based on the visual treatment of plasma flame and the dimensions determined it was seen that the thermocouple probe tips were inside the flame cross- section in the invisible reactor. The first two thermocouples were inside the main

1 flame body while the others were in the effective tail  
 2 region of the flame inside the closed reactor.



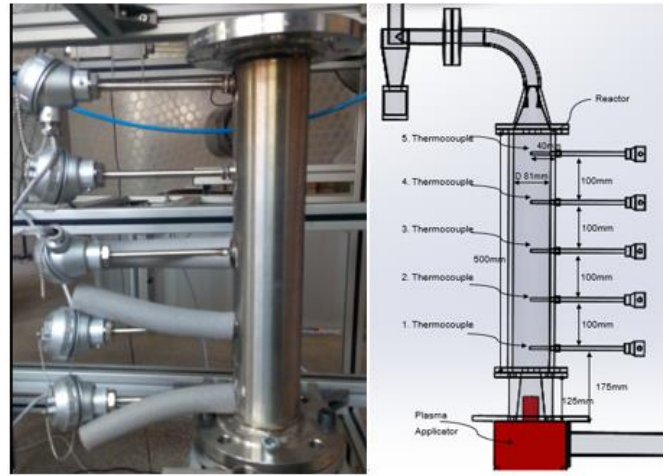
5  
 6 Fig. 1. Plasma flame as a downflow free jet in open  
 7 atmosphere at 50 L/min air with P=3600 W

8  
 9 The sketches of the reactor in the operational mode of  
 10 gasification process are given in Fig. 2. The temperature  
 11 measurements given in the paper are for the downdraft  
 12 case of the reactor with reverse of the described case in  
 13 Fig. 2 (reactor head and plasma applicator are on the top  
 14 of reactor and flame is directed as a downflow jet).

15 The temperature measurements were taken at 1 second  
 16 intervals and the data were stored in ELIMKO E-PR-110  
 17 model data acquisition card installed in a PC. Time  
 18 averaging of the collected local instantaneous  
 19 temperature data  $T=T(t)$  were used to determine the local  
 20 time- averaged flame temperature,  $T_y$  as follows:

21 
$$T_y = \frac{1}{N} \sum_{t=1}^N T(t) \quad (1)$$

22 Where N: number of thermocouple data  
 23 N is used as 300 and 1200 corresponding to the 5 min and  
 24 20 min operational time respectively.



27  
 28 Fig. 2. Reactor with thermocouple positions in the  
 29 operational mode of updraft gasification case

30  
 31 **3. Results and Discussion**

32 **3.1 The comparison of the utilized approach with the**  
**one of Padala et al. 2017 [4].** The comparison of the  
 33 utilized approach is given with the one of Padala et al.,  
 34 2017 specified in Table 2. They used Schlieren  
 35 Diagnostic System inside a closed chamber having 185  
 36 cm<sup>3</sup> volume. Spark ignition, SI followed by microwave  
 37 enhancement is the case they considered. Their frequency  
 38 is also the same as our study with 2450 MHz.  
 39

40  
 41 Table 2. Specifications of the study of Padala et al., 2017

| INPUT POWER | TYPE AND AMOUNT OF FLOW RATE                                | EXPERIMENTAL CONDITIONS                                                                                                                                        | SIZE OF FLAME                                                                                                                                                                                                                                                          |
|-------------|-------------------------------------------------------------|----------------------------------------------------------------------------------------------------------------------------------------------------------------|------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|
| P = 500 W   | Propane-Air Mixture at varying equivalence ratios up to 0.7 | -Closed chamber 185 cm <sup>3</sup><br>-SI Followed by Microwave enhancement<br>-At a pressure of 120 kPa<br>Measurement means<br>-Schlieren diagnostic system | Data at an equivalence ratio of 1 varying between D= 0.5 cm - 2 cm<br>Data at a varying equivalence ratio varying between D= 0.5cm- 1 cm<br>Data at an equivalence ratio of 0.7 varying between D= 0.5 cm- 2 cm<br>Data at a dry air varying between L= 0.2 cm- 0.6 cm |

1 Propane-Air mixture at varying equivalence ratios of  
 2 up to 0.7, equivalence ratio 1 and dry air data are referred  
 3 at a constant input power of  $P=500$  W. The listed  
 4 differences are as follows:

- 5 1. The volume of the chamber is 1/13.92 of the present  
 6 study reactor
- 7 2. The pressure is 120 kPa for their study while in the  
 8 presented study standard atmospheric pressure is used.
- 9 3. In the present study an extensive range of power ( $P$ ), is  
 10 taken into account to estimate the major influence of  
 11 power ( $P$ ) on the generated flame. 53
- 12 4. Their estimated shape of flame is spherical - elliptical  
 13 with their reference of a single size for flame. This size  
 14 is corresponding to the length of flame ( $L$ ) in the  
 15 present study. 54

16 5. Their main purpose is to determine the influence of  
 17 microwave plasma enhancement in comparison with  
 18 spark ignition only. They determined flame size and  
 19 flame speed under the influence of the equivalence  
 20 ratio primarily. 55

21 They concluded that the application of microwave  
 22 plasma enhanced the flame characteristics.

23 In reference to Table 2 Padalaet al. 2017 [4]'s range of  
 24 the estimated spherical-elliptical flame size ( $D$ ) is  
 25 between 0.2 cm - 2 cm which are much less than the ones  
 26 estimated from downflow free jet plasma flame of  
 27 cylindrical shape. In case of the same  $P=500$  W  
 28 measurements of the referred study [5] diameter ( $D$ ) is  
 29 between 1.2 cm - 1.5 cm and length ( $L$ ) is approximately  
 30 6 cm leaving the plasma applicator (of length 5 cm and  
 31 diameter 3 cm) The reason is due to the methodology  
 32 used and the case discussed. 56

33 However the determined flame speed of Padalaet al.  
 34 2017 [4] is the reference basis for the analysis of this  
 35 paper. The magnitude of flame speed they measured can  
 36 be approximated as 50 cm/s covering the flame size range  
 37 of  $1\text{ cm} < D < 2\text{ cm}$  for an equivalence ratio of 0.7. They  
 38 also noticed the change in the shape -size of plasma  
 39 kernel with the change in microwave pulse of a variable  
 40 duration used between 0.1 ms and 1.5 ms. They also  
 41 noted the difficulty of the differentiation between hot gas  
 42 and pure plasma in their approach. 57

43 **3.2 Flame generation as a function of power: used**  
 44 **methodology.** The generation of flame and therefore  
 45 flame growth is governed by the magnitude of power ( $P$ ).  
 46 The flame generation in the closed invisible reactor is  
 47 sensed by means of the measurements of thermocouples;  
 48  $T(y,t)$ . The thermocouples' recording is a timely  
 49 procedure as described by Eq. 1. In other words, thermal  
 50 characterization of the flame is done instantly. 58

51

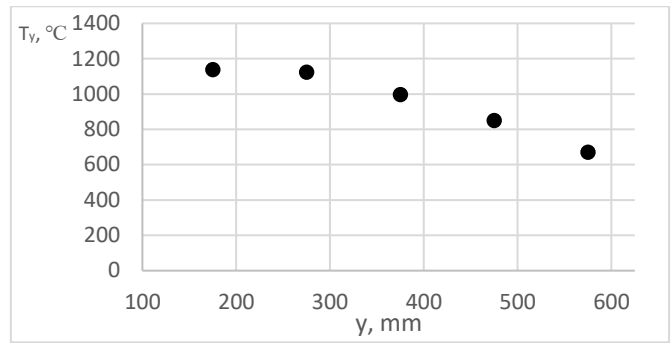


Figure 3a. Variation of  $T_y$  along flame for  $P=5400$  W at 50 L/min air

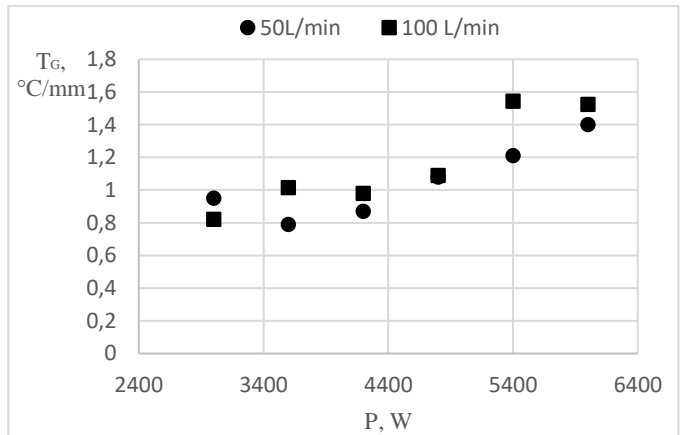


Figure 3b. Variation of TG magnitude with power ( $P$ ) for 50 L/min and 100 L/min air flow rate

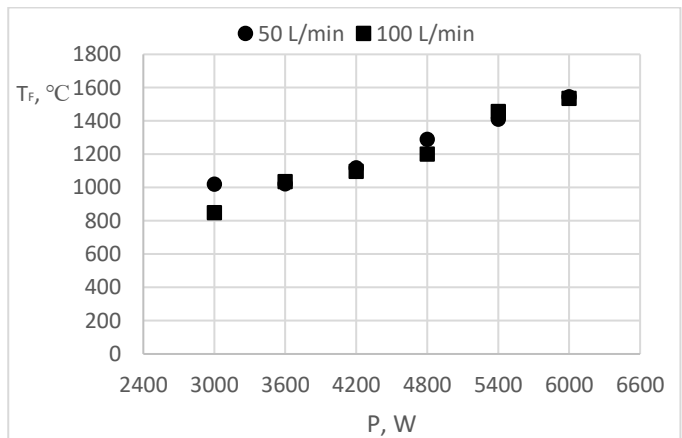


Figure 3c.  $T_F$  variation with power ( $P$ ) for 50 L/min and 100 L/min air flow rate

The generation of the plasma flame with air at the rates of 50 L/min and 100 L/min at the start of the procedure for the lowest power application of  $P=3000$  W has an operation time of 20-minute time interval. The temperature data at each power ( $P$ ) increment for  $P>3000$  W is through 5-minute time intervals for the execution of

the process. The input power is increased during the procedure covering the range  $3000 \text{ W} \leq P \leq 6000 \text{ W}$  at 600 W intervals (taking the intermediate levels of 3600W, 4200W, 4800W, 5400W). The sample data for the variation of  $T_y$  along the flame is given for  $P=5400 \text{ W}$  at 50 L/min rate of air in Fig. 3. The magnitude of  $T_y$  has a decrease along the flame with  $y$ ; for all power ( $P$ ).

As can be seen from sample plot in Fig. 3.a,  $T_y$  along flame has a linear change with  $y$  such that as  $y$  increases  $T_y$  decreases. The fitted equations have the following form:

$$T_y = TG y + T_F \quad (2)$$

Where  $T_y$  in  $^{\circ}\text{C}$  and  $y$  in mm.  $TG$  and  $T_F$  are the constants with units  $^{\circ}\text{C}/\text{mm}$  and  $^{\circ}\text{C}$  respectively defined as follows:

$$TG = dT_y / dy \quad (2.a)$$

$$T_F = (T_y)_{y=0} \quad (2.b)$$

$TG$  is defined as the temperature gradient and  $T_F$  is defined as the flame temperature at  $y=0$ . The deviation of experimental data from the estimated Eq. 2 is between the order of magnitude of  $\pm 2\%$  and  $\pm 21\%$  in the covered cases. Increased air rate results in a decrease in data scattering. The maximum data scattering is observed at the first two positions  $y=175 \text{ mm}$  and  $y=275 \text{ mm}$  since  $T_y$  almost stays constant for particularly  $P < 4200 \text{ W}$ . The values of  $TG$  and  $T_F$  are given in Table 3.

Table 3.  $TG$  and  $T_F$  values

| FLOW RATE (L/min) | POWER (W) | TG ( $^{\circ}\text{C}/\text{mm}$ ) | $T_F$ ( $^{\circ}\text{C}$ ) |
|-------------------|-----------|-------------------------------------|------------------------------|
| 50                | 3000      | -0.95                               | 1019,7                       |
| 50                | 3600      | -0.795                              | 1022                         |
| 50                | 4200      | -0.866                              | 1117,3                       |
| 50                | 4800      | -1.076                              | 1289,9                       |
| 50                | 5400      | -1.212                              | 1411,2                       |
| 50                | 6000      | -1.405                              | 1545                         |
| 100               | 3000      | -0.82                               | 848                          |
| 100               | 3600      | -1.014                              | 1035                         |
| 100               | 4200      | -0.908                              | 1096,4                       |
| 100               | 4800      | -1.085                              | 1201,6                       |
| 100               | 5400      | -1.544                              | 1456                         |
| 100               | 6000      | -1.524                              | 1535,3                       |

The ranges of the magnitudes are  $-0.795 \leq TG \leq -1.544$  and  $848 \leq T_F \leq 1545$  respectively (Fig.3b and Fig.3c).  $T_F$  shows the temperature at the center of plasma applicator as the maximum magnitude of flame temperature. It seems that at  $P = 3000 \text{ W}$ ,  $T_F = 1019 \text{ }^{\circ}\text{C}$  at 50 L/min air; increase in power ( $P$ ) to 6000 W causes an increase in  $T_F = 1545 \text{ }^{\circ}\text{C}$ . For both power ( $P$ ); at 100 L/min air the magnitudes of  $T_F$  are less than the ones with 50 L/min. Variation of  $TG$  with power ( $P$ ) for a given amount of flow rate have two confusions for 50 L/min passing from  $P = 3000 \text{ W}$  to  $P = 3600 \text{ W}$  and for 100 L/min air passing from  $P = 3600 \text{ W}$  to  $P = 4200 \text{ W}$  with decreasing magnitudes of  $TG$ .

Meanwhile  $T_F$  variation with power ( $P$ ) can be described by the following Eq. 3 irrespective of the rate of air in an approximate error band of  $\pm 5\%$

$$T_F = 0,2088 P + 275,13 \quad (3)$$

Where  $T_F$  in units  $^{\circ}\text{C}$  and  $P$  in W.

It means that irrespective of the rate of air increase in  $P$  causes increase in  $T_F$  as an expected fact.

**3.3 Modeling of microwave plasma flame: introduction of parameters.** Power sustainability of flame can be expressed through the defined parameters of thermal speed ( $VT$ ) and growth speed of flame ( $Vy$ ) besides temperature gradient ( $TG$ ). Temperature gradient ( $TG$ ) of plasma flame is a function of power ( $P$ ). A thermally stable flame generation is the case with the lowest magnitudes of  $TG$ . Thermal Speed, ( $VT$ ) is defined as the change in  $T_y$  at a location,  $\Delta T_y$  with time  $\Delta t$  for increase in power ( $\Delta P$ ) and is expressed in units of  $^{\circ}\text{C}/\text{s}$  as defined in Eq. 4.

$$VT = \Delta T_y / \Delta t \quad (4.a)$$

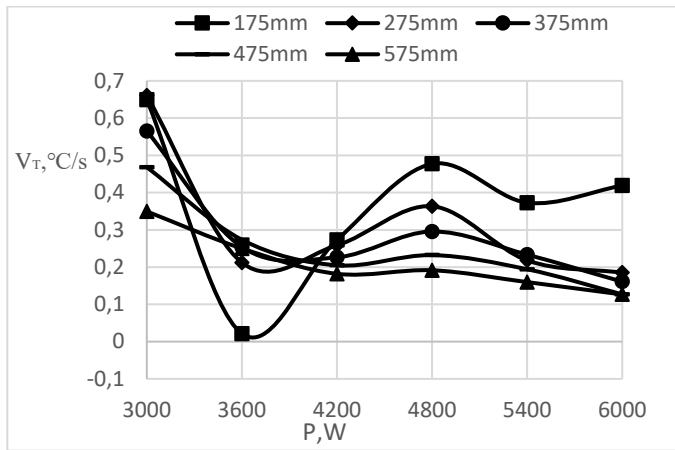
Flame Growth Speed  $Vy$  is defined as the ratio of  $VT$  to  $TG$  and expressed in units of mm/s as follows:

$$Vy = VT / TG \quad (4.b)$$

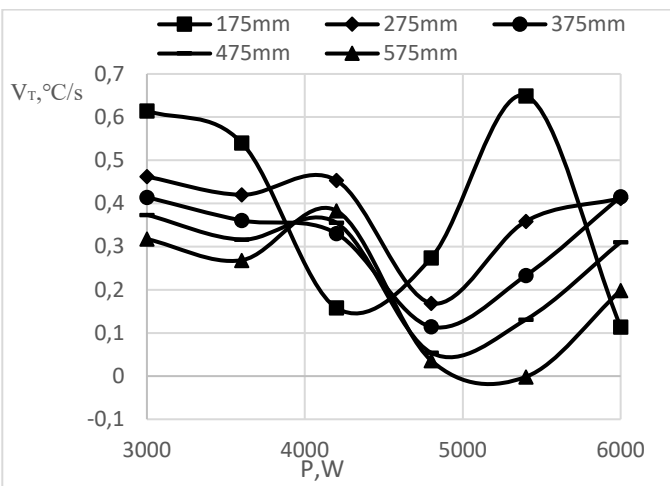
The variation of  $VT$  with power ( $P$ ) along the flame at different locations is given in Fig. 4.a and 4.b for 50 L/min and 100 L/min rates of air.

Plasma flame generation is such that 20-minute operation time was necessary for the initial temperature measurements at  $P=3000 \text{ W}$  since the reactor was at the temperature of the ambient. Therefore, the magnitudes of  $VT$  at all positions for  $P=3000 \text{ W}$  have their greatest magnitudes due to the case of the greatest magnitudes of  $\Delta T_y$  with the lowest magnitude of temperature in the reactor. The remaining temperature measurements were taken at equal 5 minute-operation time. It means that

1 from P=3000 W to P= 6000 W total operation time is 25  
 2 minutes.



4 Fig. 4a. Variation of VT with power (P) at 50 L/min air

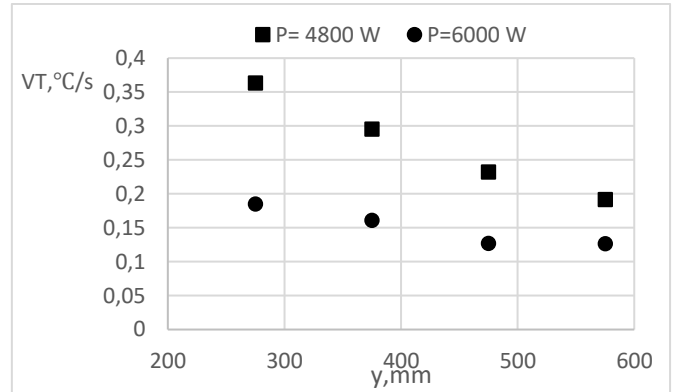


7 Fig. 4b. Variation of VT with power (P) at 100 L/min air

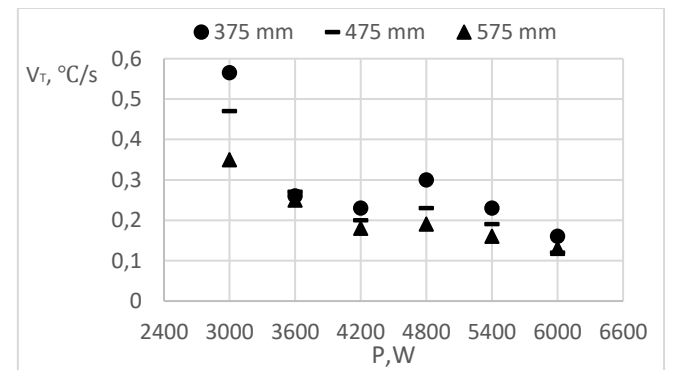
9  
 10 Therefore, the magnitude of VT is both dependent on  
 11 location and applied power. The fluctuation behavior of  
 12 VT with P at the first position,  $y= 175$  mm is due to the  
 13 generation of flame and the closeness of the location to  
 14 the plasma applicator. The magnitude of VT varies with  
 15 power (P) between  $0.66$  °C/s- $0.0214$  °C/s for 50 L/min  
 16 air and between  $0.6$  °C/s- $0.1$  °C/s for 100 L/min air flow.  
 17 Meanwhile for the other locations  $y>175$  mm particularly  
 18 for 50 L/min dependence of VT with power (P) over the  
 19 covered range of P is smooth. The magnitudes of VT at  
 20 all locations for the covered P are almost in the same  
 21 order (P= 3600 W; VT=  $0.2$  °C/s- $0.25$  °C/s, P= 4800 W;  
 22 VT=  $0.19$  °C/s- $0.36$  °C/s, P=6000 W VT=  $0.13$  °C/s- $0.18$   
 23 °C/s). It seems that increase in power (P) causes  
 24 disappearing effect of location on VT. On the other hand,  
 25 the behavior of VT with P for 100 L/min even for  $y>175$   
 26 mm has a fluctuating variation different from the one  
 27 observed in Fig. 4.a for 50 L/min air. Therefore, flame

28 has shown a better thermal performance at the lowest rate  
 29 of air.

30 In this respect for 50 L/min air the variation of VT with  
 31 y at P=4800 W and P= 6000 W is given in Fig. 5.a for  
 32  $y>175$  mm. It is seen that at P= 4800 W; VT varies  
 33 between  $0.36$  °C/s to  $0.19$  °C/s from  $y= 275$  mm to  $y=$   
 34  $575$  mm while at P=6000 W the recorded values of VT  
 35 are  $0.18$  °C/ s and  $0.126$  °C/ s.



37 Fig. 5a. Variation of VT with distance along flame at  
 38 different power (P) for 50 L/min air flow rate



39 Fig. 5b. Variation of VT with power (P) along flame at  
 40 50 L/min air flow rate

41 Increase in power (P) causes a flame stabilization with  
 42 an average and reduced value of VT over the flame.  
 43 Variation of VT with power (P) (Fig. 5.b) and variation  
 44 of  $V_y$  with P (Fig. 6) along the flame indicate at locations  
 45  $y \geq 375$  mm similar trend as decrease in the magnitudes  
 46 of VT and  $V_y$  with P as can be given in Table 4. The  
 47 magnitude of maximum  $V_y$  is  $0.56$  mm/s at P=3000 W at  
 48  $y= 375$  mm. It can be estimated that decrease in P is  
 49 associated with an increase in  $V_y$ .

50 In order to have an overall analysis Table 5 lists the  
 51 position-averaged magnitudes of VT and  $V_y$  for the  
 52 covered P range and Fig. 7 shows the relationship.  $V_y$   
 53 variation with VT can be described by the following Eq.  
 54 5 in an approximate error band of  $\pm 8$  %.

$$V_y = 1,1219 VT - 0,0286 \quad (5)$$

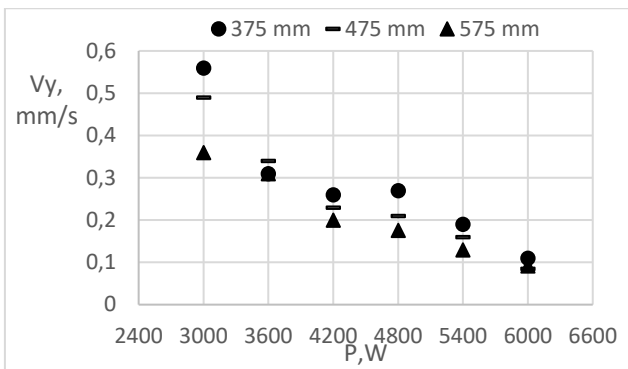


Fig. 6. Variation of  $V_y$  with power ( $P$ ) along flame at 50 L/min air flow rate

Since the magnitudes of TG in the order of 1, VT and  $V_y$  are almost identical. Meanwhile as a physical fact thermal speed and growth speed of flame are also close to each other.

Table 4. Calculated magnitudes of VT and  $V_y$

| FLOW RATE - POSITION | P (W) | VT °C/s | $V_y$ , mm/s |
|----------------------|-------|---------|--------------|
| 50 L/min - 375 mm    | 3000  | 0.565   | 0.56         |
|                      | 3600  | 0.26    | 0.31         |
|                      | 4200  | 0.23    | 0.26         |
|                      | 4800  | 0.3     | 0.27         |
|                      | 5400  | 0.23    | 0.19         |
|                      | 6000  | 0.16    | 0.113        |
| 50 L/min - 475 mm    | 3000  | 0.468   | 0.49         |
|                      | 3600  | 0.27    | 0.34         |
|                      | 4200  | 0.2     | 0.23         |
|                      | 4800  | 0.23    | 0.21         |
|                      | 5400  | 0.194   | 0.16         |
|                      | 6000  | 0.12    | 0.085        |
| 50 L/min - 575 mm    | 3000  | 0.35    | 0.36         |
|                      | 3600  | 0.25    | 0.31         |
|                      | 4200  | 0.18    | 0.2          |
|                      | 4800  | 0.19    | 0.176        |
|                      | 5400  | 0.16    | 0.13         |
|                      | 6000  | 0.13    | 0.092        |

Table 5. Position-averaged magnitudes of VT and  $V_y$  for 50 L/min

| P (W) | VT (°C/s) | $V_y$ (mm/s) |
|-------|-----------|--------------|
| 3000  | 0,46      | 0,47         |
| 3600  | 0,26      | 0,32         |
| 4200  | 0,2       | 0,23         |
| 4800  | 0,24      | 0,22         |
| 5400  | 0,19      | 0,16         |
| 6000  | 0,14      | 0,1          |

The comparison with Padala et al's magnitude of flame speed can be done as a concluding remark. Their measured speed is 50 cm/s at 500 W. However, their used time- interval is in the range of 0.1 ms and 1.5 ms. In our case 1 s is our time-interval.

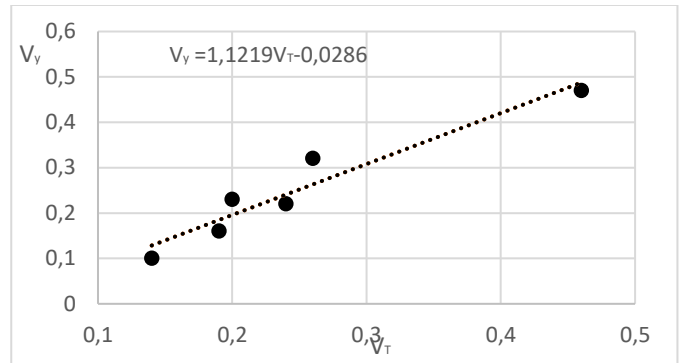


Fig. 7. Variation of  $V_y$  with VT (Position averaged at 50 L/min for covered power ( $P$ ))

Disregarding the differences of range of power and the method of measurement primarily and letting their average timing of 0.8 ms our estimated growth speed  $V_y$  can be normalized by a multiplication factor  $MF = 1/0.8 \times 10^{-3}$ .  $V_y = 0.56$  mm/s can be normalized as  $V_y = 0.56 \times MF = 700$  mm/s which is in the same order of Padala et al's magnitude.

#### 4. Conclusions and Perspectives

Microwave plasma flame generation and flame growth is modeled in this analysis as a function of power ( $P$ ) for  $P > 3000$  W.

The local temperatures inside the flame are greater with the reduced amount of air rate although increase in input power is causing an increase in the magnitudes of local temperatures. Thermal stabilization of the flame can be described by linear smooth decrease of  $T_y$  along flame. Thermal speed (VT) has shown a power stabilization of the flame for high power estimated as  $P > 4000$  W.

In spite of the differences in the studies the overall estimation on flame growth speed  $V_y$  is in conformity with the order of magnitude of Padala et al's one.

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## 1 References

- 2 [1] Aleiferis, P.G., et al. Cyclic Variations of Initial Flame Kernel  
3 Growth in a Honda VTEC-E Lean-Burn Spark-Ignition Engine.  
4 *SAE Transactions*, 109, 1340-1380, 2000.
- 5 [2] Ikeda, Y., Moon, A., and Kaneko, M. Development of microwave-  
6 enhanced spark-induced breakdown spectroscopy. *Applied Optics*,  
7 49, 13, C95-C100, 2010.
- 8 [3] Kuwahara, K. and Ando, H., *Role of Heat Accumulation by*  
9 *Reaction Loop Initiated by H<sub>2</sub>O<sub>2</sub> Decomposition for Thermal*  
10 *Ignition*. 2007, SAE International.
- 11 [4] Padala, S., Nishiyama, A., and Ikeda, Y. Flame size measurements  
12 of premixed propane-air mixtures ignited by microwave-enhanced  
13 plasma. *Proceedings of the Combustion Institute*, 36, 3, 4113-4119,  
14 2017.
- 15 [5] Sanlisoy, A. and Carpinlioglu, M.O. Preliminary measurements  
16 on microwave plasma flame for gasification. *Energy, Ecology and*  
17 *Environment*, 3, 1, 32-38, 2018.
- 18 [6] Carpinlioglu, M.O. and Sanlisoy, A. Katı Atıkların Enerji  
19 Dönüşümünde Plazma Gazlaştırma Kullanımı ile Çalışan  
20 Laboratuvar Ölçekli Bir Test Düzeneginin (Mikrodalga  
21 Gazlaştırıcı) "Mewgazlaştırıcı" Tasarım Üretim ve Performans  
22 Değerlendirilmesi-Plazma Gazlaştırma Teknolojisinin-Bilginin  
23 Üretilip Kullanılmasında Bir Vaka *TUBITAK 115M389 Final*  
24 *Report*, 2018.
- 25 [7] Sanlisoy, A. and Carpinlioglu, M.O. A review on plasma  
26 gasification for solid waste disposal. *International Journal of*  
27 *Hydrogen Energy*, 42, 2, 1361-1365, 2017.

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